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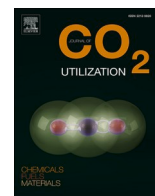
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Paradigmatic demonstration of sonochemical carbon dioxide reduction proceeded over Cu-based catalysts

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ABSTRACT

Sonochemical carbon dioxide (CO₂) reduction represents a promising decarbonization technology. However, relevant studies regarding the usage of solid catalysts in sonochemical reactor are rare. Herein, we investigate four distinct highly nanostructured cuprous oxides and sulfides for sonochemical CO₂ reduction via ultrasound-induced cavitation. Specifically, we investigate Cu₂O cubes, Cu₇S₄/Cu₂O cubes, Cu₇S₄ cages and Cu₇S₄ sheets morphologies. Each nanostructure is found to produce CO and H₂ in various ratios ranging from 1.0 – 2.3. Through a systematic study, we investigate the role of different acoustic conditions on affecting CO₂ sonolysis, involving the measurements in CO₂-saturated H₂O, 5 %CO₂/Ar-saturated H₂O, N₂-saturated H₂O, 5 %CO₂/N₂-saturated H₂O and CO₂-saturated KHCO₃. We show that Cu₂O cubes have the highest CO₂-to-CO conversion (up to 4286.4 μmol·L⁻¹·g⁻¹·h⁻¹) in 5 %CO₂/Ar-saturated H₂O. In addition, the as-synthesized Cu₂O cubes exhibited promising sonochemical stability, with CO and H₂ production rates stabilizing at around 890.3 μmol·L⁻¹·g⁻¹·h⁻¹ and 966.9 μmol·L⁻¹·g⁻¹·h⁻¹, respectively. Post sonochemical analysis indicated that the Cu₂O cubes maintain relatively high CO₂-to-CO conversion, as well as their morphology. This work provides the first proof-of-concept demonstration of using inexpensive Cu-based catalysts to enable low-carbon sonochemical CO₂ reduction.

1. Introduction

The depletion of fossil fuels alongside the accumulation of CO₂ in the atmosphere is currently leading to critical environmental issues such as global warming, ocean acidification, glacier melting, and extreme weather events [1–4]. To address these critical challenges, numerous different carbon capture and utilization technologies have been developed to convert atmospheric CO₂ into value-added products, chemicals and feedstocks [5–10]. Despite great progress, commercially available technologies for CO₂ reduction to produce fuels and chemicals remain in their infancy, motivating the scientific community to investigate alternative approaches to this conversion.

Sonochemistry has recently gained traction as an attractive approach to drive chemical transformations, such as the conversion of CO₂ into value-added chemicals and fuels [11–13]. It operates on the principle of ultrasound-induced bubble formation, growth and collapse (acoustic cavitation), driving extreme reaction conditions such as temperatures up to 5000 K and pressures up to 1000 bar which can last for a few

microseconds [14–17]. These conditions lead to the production of reactive intermediates (e.g., H•, CH₂•, HO•) [11,18], followed by initiating chemical reactions [19,20]. However, the electricity-driven yet low-carbon sonochemical CO₂ reduction reaction has not been intensively explored compared to the significant efforts dedicated to electrochemical [21], photochemical [22], thermochemical [23], biochemical [24] and piezo-photocatalytic CO₂ valorization [25,26]. Taken examples of activity improvement or catalyst preparation for boosted piezo-photocatalytic CO₂ conversion, Bi et al [26] created a dual-site of La³⁺ and Al³⁺ in SrTiO₃ via the ball-milling molten salt process, leading to the obtained catalyst showing considerably enhanced CO₂ reduction performance. Zhu et al. [25] prepared Au nanoclusters modified red graphitic carbon nitride catalyst for piezo-photocatalytic CO₂ reduction, which exposed more active Au sites resulting in improved CO production.

Previous studies have demonstrated that acoustic cavitation can drive the conversion of CO₂ into hydrocarbons, however, such studies utilized catalyst-free systems and required multivariant gases (e.g. Ar,

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He, N₂ or H₂) to activate efficient CO₂ sonolysis [27,28]. Higher solubility of CO₂ in a multivariant gas environment tends to promote bubble coalescence instead of inertially collapsing cavitation bubbles. Thus, CO₂ only saturated solutions generally have reduced sonochemical activity [19]. For example, Harada demonstrated CO₂-to-CO conversion in CO₂/Ar, CO₂/He, CO₂/H₂ or CO₂/N₂ atmospheres, whereas pure CO₂-saturated H₂O showed no evidence of CO₂ reduction [28]. Similarly, Islam et al. [27] found a dramatically lower sonochemical activity in pure CO₂-saturated H₂O compared to CO₂/H₂, CO₂/N₂, and CO₂/Ar saturated water. Notably, in this study, with the presence of H₂, hydrocarbons such as CH₄, C₂H₄ and C₂H₆ were detected. Gireesan et al. [13] adopted a diffusion limited model to simulate the collapse intensity of a single Ar-CO₂ bubble to develop fundamental insight regarding the concentration effect of dissolved CO₂ on cavitation. They observed that a higher proportion of CO₂ in the Ar/CO₂ bubble led to a significantly reduced collapse intensity, as characterized by decreased generation of radicals. In addition, a higher fraction of dissolved CO₂ resulted in enlarged bubble size containing higher water vapor concentration which resulted in a significantly decreased temperature upon collapse.

Recently, catalysts have been investigated for sonochemical CO₂ reduction. To date, such studies have demonstrated improved CO₂ reduction performance even in pure CO₂-saturated solutions (without multivariant gas environments) compared to catalyst-free sonochemical CO₂ reduction. For instance, Ma et al. [29] fabricated H₂Ti₃O₇ nanowires to conduct sonochemical CO₂ reduction for 2 h in CO₂-saturated H₂O containing sacrificial sodium sulfide and sodium sulfite, which demonstrated a marked CO production rate of 8.3 $\mu\text{mol}\cdot\text{L}^{-1}\cdot\text{g}^{-1}\cdot\text{h}^{-1}$. More recently, Babikir et al. [12] highlighted that cavitation events enabled conversion of CO₂ to multicarbon products of oxygenates (9 ppm of ethanol and 6 ppm of acetone) and acetamide (10 ppm) at 70 °C for 2 h, upon the utilization of liquid metal gallium catalysts in 20 mL CO₂-saturated H₂O containing 1 mL of NH₄OH solution. These investigations report excellent catalyst promoted CO₂ sono-reduction performance but the reported systems either needed the addition of sacrificial agents [29] or worked at an elevated temperature [12]. Evidently, the development of high-performing metal-based catalysts that can induce strong cavitation events on their own for CO₂ conversion is of crucial urgency and significance to fill in the gap [30].

Inspired by the high performance (activity, selectivity and durability) of Cu-based catalysts for electrochemical CO₂ reduction [5,31,32], herein we synthesized four Cu-based catalysts for sonochemical CO₂ reduction. Namely we prepared Cu₂O cubes, Cu₇S₄/Cu₂O cubes with a configuration of Cu₇S₄ nanosheet-shell encapsulating Cu₂O cores, Cu₇S₄ cages and Cu₇S₄ sheets. Among them, the Cu₂O cubes exhibited the most optimal CO₂-to-CO conversion in CO₂-saturated H₂O with 272.1 $\mu\text{mol}\cdot\text{L}^{-1}$ per gram catalyst ($\mu\text{mol}\cdot\text{L}^{-1}\cdot\text{g}^{-1}$) CO yield. In addition to CO, H₂ was also produced with a CO/H₂ ratio across all of the as-synthesized catalysts of 1.0–2.3 (syngas). The role of atmosphere on sonochemical CO₂ reduction performance was also investigated. We demonstrate that a dramatic sonochemical CO₂-to-CO conversion improvement was achieved, reaching 1428.8 $\mu\text{mol}\cdot\text{L}^{-1}\cdot\text{g}^{-1}$, equivalent to a CO production rate of 4286.4 $\mu\text{mol}\cdot\text{L}^{-1}\cdot\text{g}^{-1}\cdot\text{h}^{-1}$, upon using 5 % CO₂/Ar-saturated H₂O. To understand the durability of the Cu₂O cubes for sonochemical CO₂ reduction, long-term experiments were conducted. The Cu₂O cubes catalysts experienced only slight morphological deformation during the 40-minute test, with relatively small changes to the CO₂ reduction activity during CO₂ sonolysis. This work highlights the opportunity to develop various Cu-based catalysts for converting CO₂ into high-value chemicals via sonochemistry.

2. Materials synthesis

2.1. Catalyst synthesis

Cu-based catalysts were synthesized following literature protocols with slight modifications [33]. Specifically, the Cu₂O cubes were

synthesized by dissolving Cu(CH₃COO)₂ (2.9946 g) in a beaker containing deionized H₂O (50 mL) at 70 °C with continuous stirring. Subsequently, 30 mL of 3 mol·L⁻¹ NaOH was added to the beaker dropwise to produce dark precipitates, and the mixed solution stirred for a further 20 min. Glucose powder (0.6 g) was then added with constant stirring. The wet Cu₂O cubes precipitates were washed using deionized H₂O and ethanol and dried overnight at 60 °C to obtain the Cu₂O cubes. To synthesize the Cu₇S₄/Cu₂O cubes, 0.36 g Na₂S and 0.006 g NaOH were dissolved in 150 mL anhydrous ethanol solution, followed by adding 0.6 g of the obtained Cu₂O cubes catalysts to the as-prepared solution with a continuous stirring for 10 min. The resultant black precipitates were washed by deionized H₂O and ethanol, followed by centrifugation and drying at 60 °C. The Cu₇S₄ cages catalysts were synthesized by dispersing the obtained Cu₇S₄/Cu₂O cubes in NH₃·H₂O solution (25 %) for 3 days to remove the Cu₂O core; centrifuging and washing with deionized water and anhydrous ethanol; and drying overnight at 60 °C. To produce the Cu₇S₄ sheets, 25 mL of *n*-propanol and 25 mL of deionized H₂O were added to the NH₃·H₂O solution (25 %), followed by stirring and sonication. The precipitate was washed, centrifuged and dried as described above.

2.2. Materials characterization

X-ray diffraction (XRD) patterns were collected on the powder X-ray diffractometer (PANalytical X'pert) using Cu K α source ($\lambda = 1.5406 \text{ \AA}$). Scanning electron microscopic (SEM) images were taken by a Zeiss Sigma 300 microscope (Oxford Instruments). Scanning electron microscope-energy dispersive X-ray (SEM-EDX) images were collected by the Zeiss Crossbeam 350 FIB-SEM (Zeiss Crossbeam). The particle size of as-synthesized catalysts was statistically analyzed by ImageJ. X-ray photoelectron spectroscopy (XPS) was collected at the Kratos Analytical (a Shimadzu group company), AXIS Supra+. The collected XPS spectra were then calibrated based on the C 1 s spectrum at a binding energy of 284.8 eV.

2.3. Sonochemical CO₂ reduction

Sonochemical CO₂ reduction was performed in a customized cylindrical sonochemical reactor (Figure S1). Detailed information about the reactor is provided in a previous study [17]. In brief, an air-tight vial (5 mL PPE test tube) equipped with a syringe was used as the container to store 2.5 mL of liquid solution and 5 mg catalyst. Prior to CO₂ sonocatalysis, the reactor solution was saturated with gas (e.g., pure CO₂, 5 %CO₂/Ar, 5 %CO₂/N₂, or N₂) for 15 min. The samples were exposed to ultrasound followed by cavitation in the cylindrical sonochemical reactor for 20 min under peak to peak drive voltage of 251 V (parameters of KEYSIGHT 33600 A waveform generator: frequency of 1.076 MHz; cycle count of 100; and burst period of 1.000 ms). Post sonication, the reactor valve of the equipped syringe was switched on to draw the gases from the headspace to be analyzed by gas chromatography (Shimadzu GC-2030). Nuclear magnetic resonance (NMR) was utilized to detect liquid products (JEOL JNM-ECZR 500 MHz spectrometer). Specifically, the reaction mixtures were centrifuged to separate catalysts as precipitates, and the supernates (0.5 mL) mixed with 0.15 mL of D₂O and 0.1 mL of DMSO for NMR measurement. To assess the stability of the sonocatalysis, the experiment was extended for various time intervals (5 min, 10 min, 30 min and 40 min), with all other parameters unchanged as-described above. The detailed methods to calculate the yielded products and product yield rates are provided in the [Supporting Information](#).

3. Results and discussion

3.1. Characterization of as-synthesized catalysts

To explore the efficacy of Cu-based catalysts for sonochemical CO₂

reduction, various nanostructured copper oxide and sulfide materials were synthesized. Specifically, Cu₂O cubes, Cu₇S₄ shell-Cu₂O cube core (abbreviated as Cu₇S₄/Cu₂O cubes), Cu₇S₄ cages and Cu₇S₄ sheets (Fig. 1a) were prepared following literature methods [33]. The morphologies and chemical compositions of the as-synthesized catalysts were confirmed by electron microscope imaging and energy dispersive X-ray spectroscopy (SEM-EDX) (Fig. 1b-e).

The crystal structures of the synthesized catalysts were assessed by XRD (Fig. 1h). Specifically, the as-synthesized Cu₂O cubes exhibit cubic morphologies with a roughened surface (Fig. 1b), with an average particle size of 827 ± 134 nm. The Cu₇S₄/Cu₂O cubes' surface is decorated with highly roughened Cu₇S₄ nanosheets which encapsulate the Cu₂O core (Fig. 1c), exhibiting an enlarged particle size of 1034 ± 128 nm. Cu₇S₄ cages (prepared by dissolution of the Cu₂O core) are hollow structures (Fig. 1d), with an averaged particle size of 943 ± 171 nm. Finally, the collapse of Cu₇S₄ cages results in the formation of smaller and agglomerated nanostructures compared to the other structure, featuring apparent agglomerated sheet morphology, thus denoted as

Cu₇S₄ sheets for simplicity (Fig. 1e). The as-synthesized Cu₇S₄ sheets featured a single sheet size of 135 ± 26 nm (Figure S2). SEM-EDX mapping was conducted on the Cu₂O cubes and Cu₇S₄ sheets, to confirm the conversion of Cu₂O to Cu₇S₄. As expected, for all measured Cu₂O, a uniform distribution of Cu was observed (Fig. 1f). Similarly, a uniform Cu and S distribution was observed in the Cu₇S₄ sheets (Fig. 1g), confirming the formation of copper sulfide material (Fig. 1h).

To probe the crystallinity of the samples, XRD was performed. The diffraction pattern for Cu₂O cubes contain pronounced diffraction peaks of (110), (111), (200), (211), (220), (311) and (222) (PDF#05-0667 Cu₂O), indicating a Cu₂O cubic structure. In addition, a low intensity peak at 38.8° is observed and assigned to the (111) plane of CuO. XRD also verified the presence of Cu₇S₄ monoclinic structure in Cu₇S₄/Cu₂O cubes, Cu₇S₄ cages and Cu₇S₄ sheets. As to Cu₇S₄/Cu₂O cubes, only (040) and (304) (PDF#33-0489 Cu₇S₄) diffraction peaks of Cu₇S₄ were observed. Conversely, for both Cu₇S₄ cages and Cu₇S₄ sheets multiple diffraction peaks are observed, including (013), (022), (113), (004), (104), (031), (302) and (422) (PDF#33-0489 Cu₇S₄).

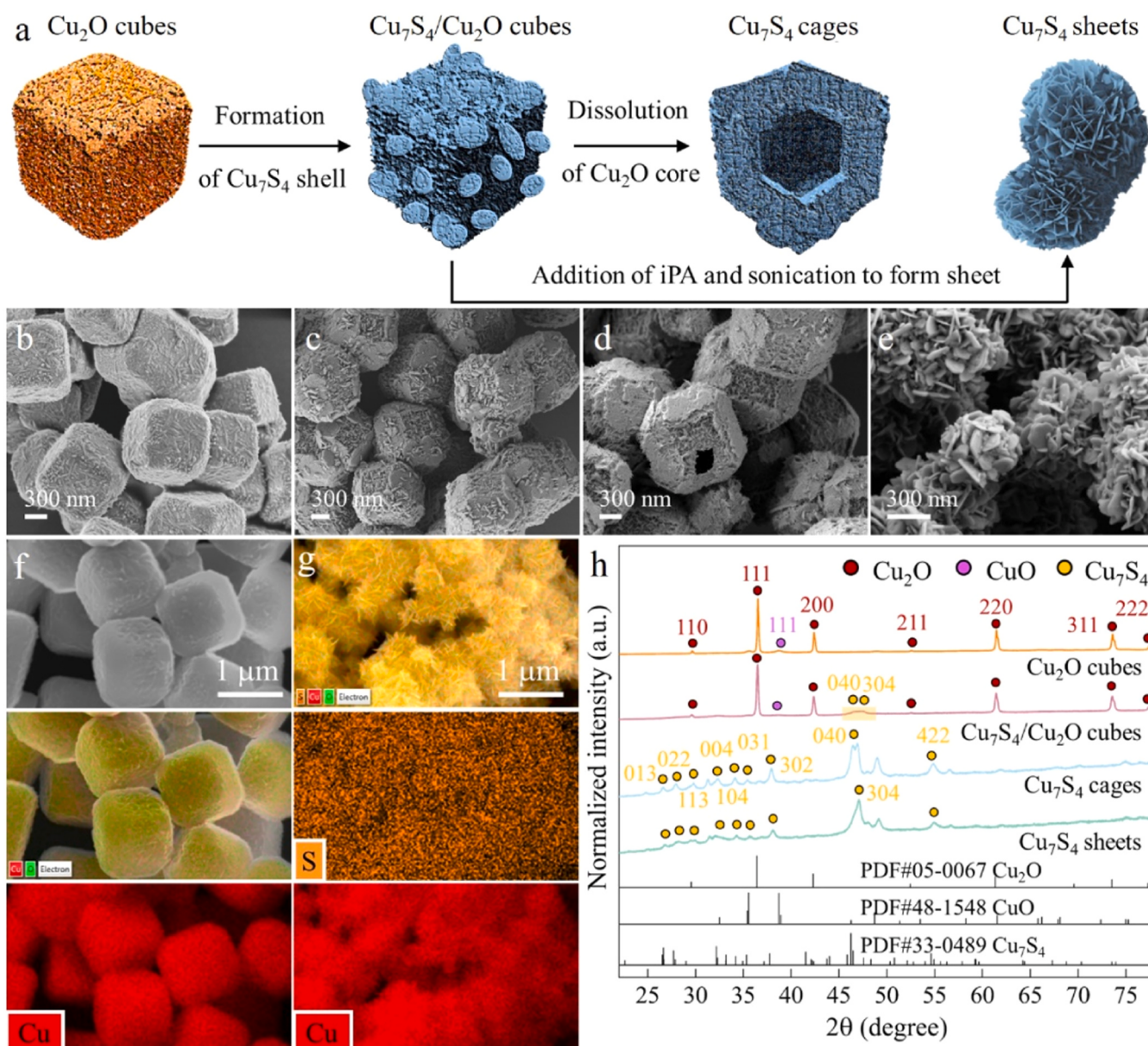


Fig. 1. (a) Schematic of the synthetic methods to prepare Cu₂O cubes, Cu₇S₄/Cu₂O cubes, Cu₇S₄ cages and Cu₇S₄ sheets. SEM images of Cu₂O cubes (b), Cu₇S₄/Cu₂O cubes (c), Cu₇S₄ cages, (d) and Cu₇S₄ sheets. (e) SEM-EDX mapping images of (f) Cu₂O cubes and (g) Cu₇S₄ sheets. (h) XRD patterns of the as-synthesized catalysts.

3.2. Evaluation of sonochemical CO₂ reduction

Sonochemical CO₂ reduction was performed in a gas-tight vial containing catalyst and various gas-saturated solutions. Prior to introducing the catalyst particles, a catalyst-free CO₂-saturated H₂O solution was first sonicated. No products were detected, confirming that any subsequent CO₂ conversion was dependent on the added catalysts. This was consistent with literature reports which have reported that highly soluble CO₂ causes increased bubble-bubble coalescence leading to highly suppressed sonochemical activity [11,27,34].

All four catalysts were shown to be active for sonochemical CO₂ reduction, producing CO and H₂ only under CO₂ saturated conditions (catalyst loading of 2 mg·mL⁻¹). Specifically, the Cu₂O cubes yielded 272 μmol·L⁻¹·g⁻¹ of CO and 270.4 μmol·L⁻¹·g⁻¹ of H₂, and the CO/H₂ ratio of was 1.0 (Fig. 2a). These observed results affirmed that the usage of Cu-based catalysts are able to significantly improve the sonochemical CO₂ reduction performance, unlike previously reported catalyst-free CO₂ sonolysis systems that required complex atmospheres to acquire effective CO₂ reduction sonocativity [11]. On top of the marked improvements in CO₂ reduction performance, the power input used in our customized cylindrical sonochemical reactor was only 20.2 W, which was substantially lower than the power of 77.8 W needed in previously reported CO₂ sonolysis system containing no catalysts [27].

The Cu₂O cubes exhibited the highest CO yields (272.1 μmol·L⁻¹·g⁻¹), followed by Cu₇S₄ sheets (177.4 μmol·L⁻¹·g⁻¹), Cu₇S₄/Cu₂O cubes (164.3 μmol·L⁻¹·g⁻¹) and Cu₇S₄ cages (101.8 μmol·L⁻¹·g⁻¹). The CO/H₂ ratio across all of the tested catalysts fell within the typical range for syngas (1.0, 1.6, 2.3 and 1.5 for Cu₂O cubes, Cu₇S₄/Cu₂O cubes, Cu₇S₄ cages and Cu₇S₄ sheets, respectively, Fig. 2b) [35–37]. As the CO/H₂ ratios range between 1.0 and 2.3, the sonochemically derived syngas can be used for the industrial Fischer-Tropsch

processes that typically need a syngas with the CO/H₂ ratio spanning from 0.5 and 2.0 to manufacture high-value chemical compounds such as CH₄ and long-chain hydrocarbons [35–37]. Owing to the high energy of sonochemical processes which result in high temperatures (~5000 K) and pressures (~1000 bar), it is critical to investigate catalyst stability during sonolysis [38,39]. SEM was used to investigate the morphological integrity of catalysts (Fig. 1b–e, and Fig. 2b). Interestingly, the more active catalysts (Cu₂O cubes and Cu₇S₄ sheets) had only slight morphological deformation post sonolysis. Conversely, the two catalysts with lower activities (Cu₇S₄/Cu₂O cubes and Cu₇S₄ cages) displayed significant morphological deformations. Whisker-like structures develop at the surface post CO₂ reduction when comparing Fig. 1b and c with corresponding post sonolysis images in Fig. 2b (two images at the center). To assess the crystal structures of the catalysts as a function of sonolysis, XRD patterns of the spent catalysts were collected (Figure S3). No significant changes in XRD patterns were observed post sonolysis for the more active Cu₂O cubes and Cu₇S₄ sheets (Fig. 1d and Figure S3). In comparison, XRD patterns of the less active Cu₇S₄/Cu₂O cubes and Cu₇S₄ cages show distinctly apparent crystal structure evolution during CO₂ sonolysis (Fig. 1d and Figure S3). We therefore hypothesize that the morphological and crystallographic deformation in Cu₇S₄/Cu₂O cubes and Cu₇S₄ cages resulted in lower CO₂-to-CO conversion.

3.3. Performance optimization of sonochemical CO₂ reduction

To further improve the sonochemical CO₂ conversion performances via reaction condition optimizations, a broad spectrum of reaction conditions were investigated utilizing the two highest performance catalysts established through the initial screening (Cu₂O cubes and Cu₇S₄ sheets). Specifically, different concentrations of KHCO₃ solutions (0.1 M, 0.3 M and 0.5 M) and reaction atmospheres (e.g. 5 %CO₂/Ar,

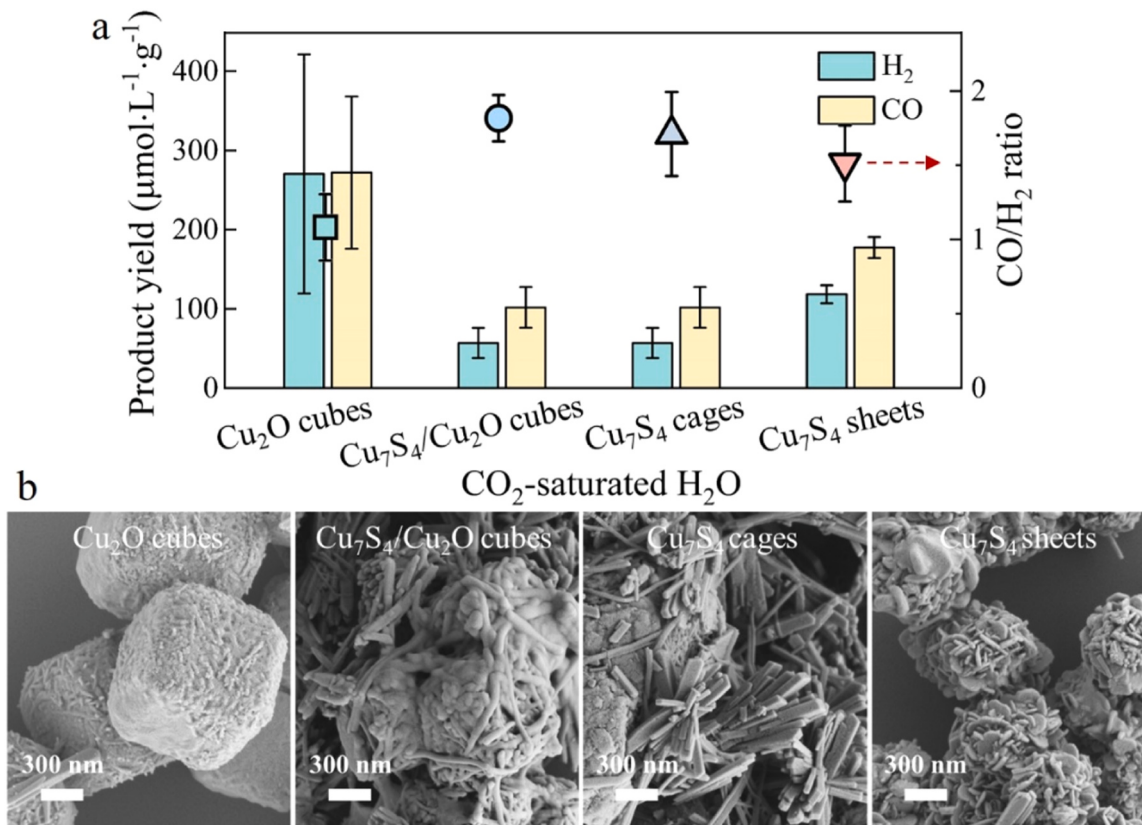


Fig. 2. (a) Product yields and measured CO/H₂ ratio in CO₂-saturated H₂O, for the four synthesized catalysts with a catalyst loading of 2 mg·mL⁻¹ (Cu₂O cubes, Cu₇S₄/Cu₂O cubes, Cu₇S₄ cages and Cu₇S₄ sheets). (b) Corresponding SEM images of Cu₂O cubes, Cu₇S₄/Cu₂O cubes, Cu₇S₄ cages and Cu₇S₄ sheets after 20 min sonochemical CO₂ reduction.

5 %CO₂/N₂ and N₂) were investigated. As shown in Fig. 3a, both Cu₂O cubes and Cu₇S₄ sheets demonstrate a lower CO₂-to-CO conversion rate in CO₂-saturated KHCO₃ solutions (regardless of concentrations) when compared to CO₂-saturated H₂O. The reduced CO₂-to-CO conversion performance in CO₂-saturated KHCO₃ solutions may be due to the increased CO₂ solubility and solution viscosity which likely leads to a reduced amount of inertial cavitation bubbles [27].

It is notable that Ar is commonly used in the literature to improve the chemical effects of cavitation. This is reportedly due to it being a monoatomic gas with a higher polytropic ratio ($\gamma=1.66$) and a lower thermal conductivity ($\lambda=0.018 \text{ W}\cdot\text{m}^{-1}\cdot\text{K}^{-1}$) [27,40]. These properties boost inertial cavitation, increasing the temperature of the bubble during collapse, and in turn, lead to increased sonochemical activity [19]. As expected, the CO₂-to-CO conversion in 5 %CO₂/Ar-saturated H₂O further increased up to $1428.8 \mu\text{mol}\cdot\text{L}^{-1}\cdot\text{g}^{-1}$ (Fig. 3a), which was more than five times higher than the CO₂-saturated H₂O ($272.1 \mu\text{mol}\cdot\text{L}^{-1}\cdot\text{g}^{-1}$). These results corroborate with previously reported catalyst-free system involving the usage of Ar to boost CO₂ sonolysis [28].

Under 5 %CO₂/N₂-saturated H₂O, no CO was observed with H₂ as the only product (Fig. 2b). This can be attributed to the lower polytropic ratio ($\gamma=1.40$) of N₂ and a higher thermal conductivity ($\lambda=0.024 \text{ W}\cdot\text{m}^{-1}\cdot\text{K}^{-1}$) compared to Ar [40]. As expected, no CO was produced in N₂-saturated H₂O reaction (Fig. 3a) because the reactant CO₂ was absent. However, the H₂ production performance improved considerably compared to Ar-free atmospheres, indicating that Cu₂O cubes catalysts can also be utilized for sonochemical H₂ production. Interestingly, 5 %CO₂/N₂-saturated H₂O (Fig. 3d) suppressed H₂ generation in comparison to 5 %CO₂/Ar-saturated H₂O and N₂-saturated H₂O, suggesting that the H₂ production rate can be controlled by changing the gaseous atmospheres upon using the Cu₂O cubes catalysts, further demonstrating the catalytic multifunctionality of the Cu₂O cubes catalysts.

To further understand the differences in CO₂-to-CO conversion as a function of reactor environments, the catalyst morphology and crystalline structure were characterized post-reaction by SEM and XRD. The highest performing catalyst (Cu₂O cubes) and reaction conditions (5 % CO₂/Ar-saturated and N₂-saturated H₂O conditions), demonstrates a stable morphology post sonolysis (Fig. 3c and Fig. 3e). In stark

comparison, the CO₂-saturated KHCO₃ solutions (Figs. 3f-3h) caused significant morphological deformations of Cu₂O cubes compared to that of CO₂-saturated H₂O (Fig. 3b). Such morphological deformations likely contributed to the deterioration of CO₂-to-CO conversion (Fig. 3a). The preservation of the catalyst morphology and crystal structure provided additional evidence to underscore the importance of structural integrity for sonochemical CO₂ reduction, which aligned with the conclusions resulting from CO₂-saturated H₂O experiments discussed in the previous section. XRD (Figure S4) confirmed that the bulk Cu₂O crystallinity was retained for all reaction conditions, and only slight crystallite size changes were observed post sonolysis.

3.4. Evaluation of the stability of catalysts

Cu₂O cubes exhibited the highest CO₂-to-CO conversion performance in CO₂-saturated H₂O, and therefore its long-term operation was assessed. As presented in Fig. 4, the catalyst is shown to be active throughout the duration of the stability measurements, producing both CO and H₂. The quantity of CO and H₂ reached $605.1 \mu\text{mol}\cdot\text{L}^{-1}\cdot\text{g}^{-1}$ and $685.3 \mu\text{mol}\cdot\text{L}^{-1}\cdot\text{g}^{-1}$, respectively, within 40 min. Rates for production of CO and H₂ ($890.3 \mu\text{mol}\cdot\text{L}^{-1}\cdot\text{g}^{-1}\cdot\text{h}^{-1}$ and $966.9 \mu\text{mol}\cdot\text{L}^{-1}\cdot\text{g}^{-1}\cdot\text{h}^{-1}$,

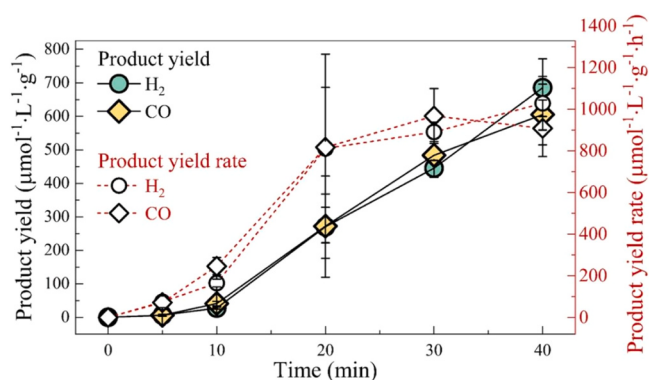


Fig. 4. Sonochemical stability testing of the Cu₂O cubes catalysts in CO₂-saturated H₂O.

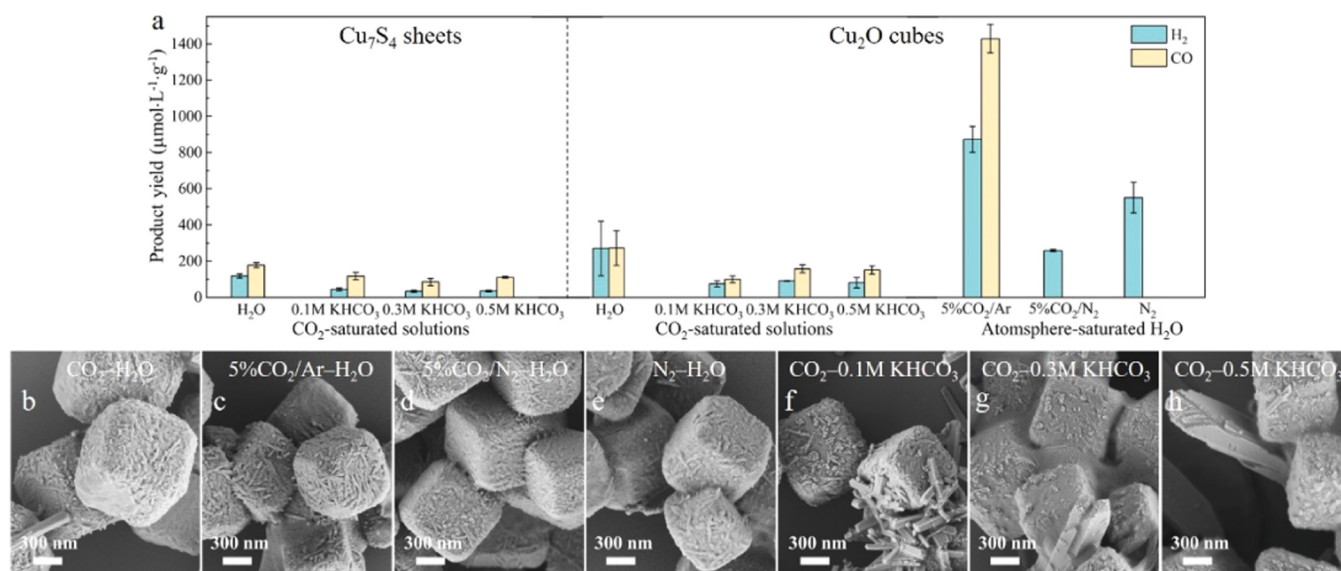


Fig. 3. (a) Product distribution analysis of sonochemical CO₂ reduction of Cu₂O cubes and Cu₇S₄ sheets operated in different reaction conditions, with the optimal Cu₂O cubes being additionally measured in 5 %CO₂/Ar-saturated H₂O, 5 %CO₂/N₂-saturated H₂O and N₂-saturated H₂O. Corresponding SEM images of Cu₂O cubes collected after sonochemical CO₂ reduction in various reaction conditions, including CO₂-saturated H₂O (b), 5 %CO₂/Ar-saturated H₂O (c), 5 %CO₂/N₂-saturated H₂O (d), N₂-saturated H₂O (e), CO₂-saturated 0.1 M KHCO₃ (f), CO₂-saturated 0.3 M KHCO₃ (g) and CO₂-saturated 0.5 M KHCO₃ solutions (h).

respectively) reached equilibrium after 30 min of operation. The average CO/H₂ ratio was 0.9 which is again within the accepted range for syngas.

To assess the Cu₂O cubes' stability as a function of time, the morphology, crystallinity and composition were characterized after 20 mins reaction in CO₂-saturated H₂O and 5 %CO₂/Ar-saturated H₂O. Slight morphology deformation was observed after sonolysis in CO₂-saturated H₂O (Fig. 5a-b and Figures S5-S6), whereas the morphology seemed unaltered in 5 %CO₂/Ar-saturated H₂O (Fig. 5c). XRD (Fig. 5d and Figure S7) showed no apparent changes to crystallinity in either experiment. XPS Cu LMM spectra (Fig. 5e) confirmed that Cu⁺ species (~569.0 eV) were prevalent in all catalysts (pre and post sonolysis), in line with the crystal phases from the XRD patterns [41]. Further analysis of the XPS Cu 2p region (Fig. 5f) evidences the co-existence of Cu²⁺ (~934.7 eV and 954.9 eV corresponding to Cu 2p_{3/2} and Cu 2p_{1/2} respectively) and Cu⁺ (~932.4 eV in the Cu 2p_{3/2} region and 952.4 eV in the Cu 2p_{1/2} respectively) species [42], with slight variations of Cu⁺/Cu²⁺ ratio after reaction in CO₂-saturated H₂O and 5 %CO₂/Ar-saturated H₂O (Table S1). Specifically, the original Cu⁺/Cu²⁺ ratio in as-synthesized Cu₂O cube was 0.35, with only a slight reduction to 0.32 and 0.34 after reaction in CO₂-saturated H₂O and 5 %CO₂/Ar-saturated H₂O, respectively, indicating the structural stability of the Cu₂O cubes catalysts, in good agreement with the XRD and SEM data.

3.5. Proposed sonochemical CO₂ reduction mechanisms

Unveiling the syngas formation pathways over the Cu₂O cube sonocatalyst is of essential importance to further optimize the CO₂ reduction efficiency. CO₂ can be directly reduced on Cu₂O surface to produce CO via CO₂ → O + CO as reported [27]. Beyond that, various radicals will be spontaneously generated in the vicinity of the Cu₂O cubes. With respect to H₂ formation, H₂O is initially decomposed via H₂O → HO• + H• to produce H• radicals, followed by H• + H• → H₂ to synthesize H₂ [28]. Alternatively, CO₂ can be reduced by the generated H• radicals spontaneously to generate CO via CO₂ + H• → CO₂H• + H• → H₂O + CO [27]. Based on these understandings, a schematic illustration of syngas formation over the Cu₂O cube triggered by ultrasound-formed bubble collapse is proposed and shown in Fig. 6. The enhancement of the effects of cavitation is vital to strengthen CO₂ reduction efficiency. Thus, future studies should explore stable porous Cu₂O catalysts or optimized sonochemical systems. This study shows the first proof-of-concept demonstration of using inexpensive Cu-based catalysts for sonochemical CO₂ reduction, verifying that Cu-based materials are also highly effective catalysts that can be deployed for CO₂ reduction via the electricity-driven green acoustic cavitation methodology.

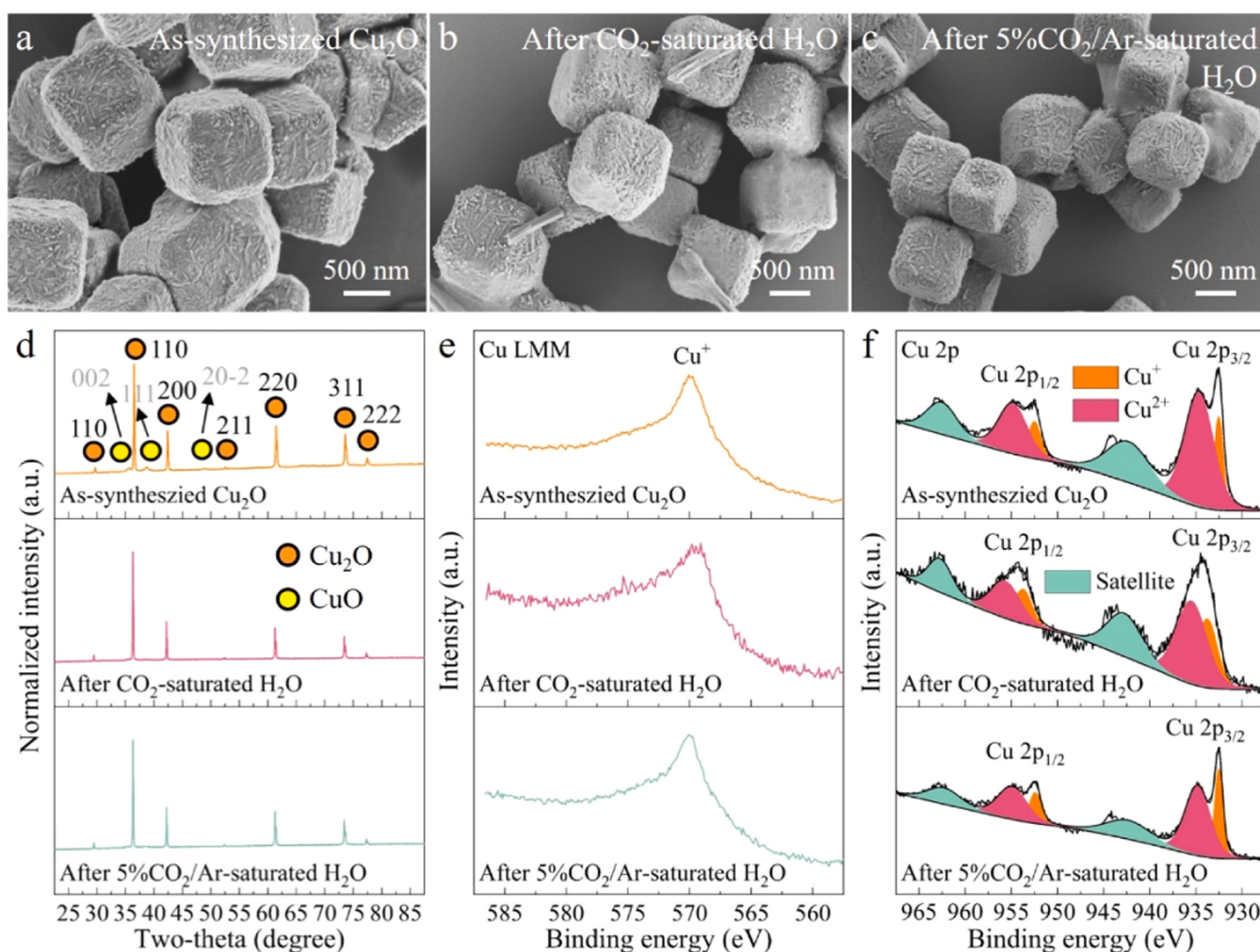


Fig. 5. SEM images of as-synthesized Cu₂O cubes (a), after 20 mins sonochemical CO₂ reduction in CO₂-saturated H₂O (b) and 5 %CO₂/Ar-saturated H₂O (c). XRD patterns (d), XPS Cu LMM spectra (e) and Cu 2p spectra (f) of as-synthesized Cu₂O cubes, after sonochemical CO₂ reduction in CO₂-saturated H₂O and 5 %CO₂/Ar-saturated H₂O.

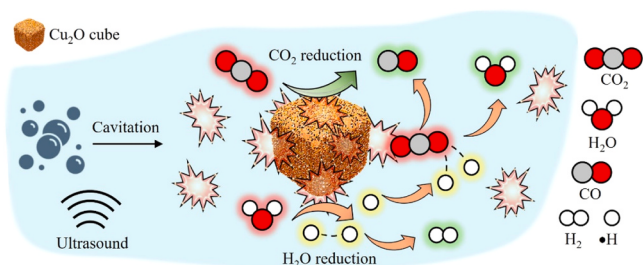


Fig. 6. Schematic demonstration of the proposed sonochemical CO₂ reduction mechanism over Cu₂O cube catalyst to produce syngas, profiling direct CO₂ reduction to CO and H₂O reduction formed H• radicals to reduce CO₂ to CO as well as to form H₂.

4. Conclusions

In this work, four Cu-based catalysts with varied compositions and morphologies were investigated for sonochemical CO₂ reduction. Namely Cu₂O cubes, Cu₇S₄/Cu₂O cubes, Cu₇S₄ cages and Cu₇S₄ sheets catalysts. Furthermore, a range of atmospheres and KHCO₃ solutions were systematically explored to assess their sonochemical CO₂ reduction performance towards preferential CO production. All catalysts were shown to be active producing both CO and H₂ under CO₂- and CO₂/Ar-saturated solutions. The CO/H₂ ratio ranged between 1.0 and 2.3 which is within the typical range for syngas. Among the tested catalysts, Cu₂O cubes revealed both the highest activity and stability regarding CO₂ to CO conversion, leading to a marked CO production yield of 272.1 $\mu\text{mol}\cdot\text{L}^{-1}\cdot\text{g}^{-1}$ in CO₂-saturated H₂O. Further measurements in 5 %CO₂/Ar-saturated H₂O significantly enhanced the CO₂-to-CO conversion performance, reaching 1428.8 $\mu\text{mol}\cdot\text{L}^{-1}\cdot\text{g}^{-1}$, equivalent to a CO production rate of 4286.4 $\mu\text{mol}\cdot\text{L}^{-1}\cdot\text{g}^{-1}\cdot\text{h}^{-1}$. Interestingly, the less active Cu₇S₄/Cu₂O cubes and Cu₇S₄ cages catalysts were found to have significant structural deformations post testing, while the most active Cu₂O cubes largely retained their structure. Similarly, when the higher performing Cu₂O cube catalysts were assessed in a range of CO₂-saturated KHCO₃ solutions, the lowest performing environments were shown to result in the highest structural deformations. This work demonstrates that the inexpensive and scalable Cu-based catalysts have the potential to drive CO₂-to-CO conversion via sonochemistry if further optimizations are carried out to generate materials that retain their structural properties during sonolysis.

CRediT authorship contribution statement

Dong Xia: Writing – review & editing, Writing – original draft, Methodology, Data curation, Conceptualization. **James Kwan:** Writing – review & editing, Supervision, Funding acquisition, Conceptualization. **King Laurie:** Writing – review & editing, Supervision, Resources, Methodology, Funding acquisition, Conceptualization. **Regmi Yagya:** Writing – review & editing, Supervision, Resources, Conceptualization. **Yi Qin:** Writing – review & editing, Methodology, Data curation.

Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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Appendix A. Supporting information

Supplementary data associated with this article can be found in the online version at doi:10.1016/j.jcou.2025.103220.

Data Availability

Data will be made available on request.

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