

## Please cite the Published Version

Joseph, Ifeoma V, Roncaglia, Giulia, Tosheva, Lubomira and Doyle, Aidan M (10) (2019) Waste peat ash mineralogy and transformation to microporous zeolites. Fuel Processing Technology, 194. ISSN 0378-3820

DOI: https://doi.org/10.1016/j.fuproc.2019.106124

Publisher: Elsevier BV

Version: Accepted Version

Downloaded from: https://e-space.mmu.ac.uk/623158/

Usage rights: Creative Commons: Attribution-Noncommercial-No Derivative Works 4.0

**Additional Information:** This is an Author Accepted Manuscript of a paper accepted for publication in Fuel Processing Technology, published by and copyright Elsevier.

## Enquiries:

If you have questions about this document, contact openresearch@mmu.ac.uk. Please include the URL of the record in e-space. If you believe that your, or a third party's rights have been compromised through this document please see our Take Down policy (available from https://www.mmu.ac.uk/library/using-the-library/policies-and-guidelines)

- 1 Waste peat ash mineralogy and transformation to microporous zeolites Ifeoma V. Joseph, Giulia Roncaglia, Lubomira Tosheva, Aidan M. Doyle\* 2 3 Department of Natural Sciences, Manchester Metropolitan University, Chester St., 4 Manchester, M1 5GD, United Kingdom. 5 6 \* Corresponding author: a.m.doyle@mmu.ac.uk 7 8 9 Abstract 10 The combustion of peat fuel for industrial scale power generation and domestic heating produces toxic ash, most of which is presently buried in landfill. In this study, the mineralogy 11 of waste peat ash was determined, followed by its successful use as a starting reagent to prepare 12 13 zeolites. X-ray diffraction (XRD) confirmed the presence of quartz, anhydrite, calcite, lime, merwinite and magnetite in peat ash, and that a single extraction step using mineral acid was 14 15 sufficient to remove all non-quartz crystal phases. Alkali fusion of the acid-extracted samples produced GIS-type zeolite. LTA- and FAU-type were also prepared by altering the Si/Al ratio 16 and extending the ageing time. Experiments confirmed that the LTA- and FAU-type zeolites 17 were active in the simultaneous adsorption of lead, cadmium, cobalt, zinc and copper from 18 aqueous solutions, with similar quantities of metals removed to those using a reference zeolite. 19 20 Keywords; Peat ash utilisation; zeolite; pyrolysis; waste management; water purification. 21 22 23
- -
- 24
- 25

## 26 **1. Introduction**

Peat is a carbon based material produced from partially decayed vegetation that builds up over 27 a duration typically up to approximately 12,000 years [1,2]. The deficiencies of oxygen and 28 29 nutrients in waterlogged bogs and fens (peatlands) limit the decay rate of vegetation such that there is an accumulation of peat over time. These peatlands cover an estimated global area of 30 4m km<sup>2</sup>, which equates to 2-3% of the total land area, and are found mainly in Russia, North 31 and South America, Northern Europe and South-East Asia, including lower quantities in 32 locations such as central Africa [1,2]. Peat is classified as an intermediate fuel i.e. between 33 34 biomass and fossil fuel (lignite). Total global consumption is estimated at 17m tons per annum, over 99% of which is used in Northern Europe for the production of heat and electricity [3]. 35 Ireland is the largest user, consuming 3.8m tons annually from peatlands that cover 36 37 approximately 20% of the national land area [4]. Most of this is used in thermal power plants to generate 8.5% of Ireland's electricity [5,6]. While renewable fuel sources are increasingly 38 being used as a substitute for peat (at least partially in the short term), the production of 39 40 electricity in Ireland using peat based fuel is an established industry with a secure, indigenous energy source, and will, therefore, continue for the foreseeable future. 41

42 Peat ash is the main waste product of combustion at thermal power stations, some of which is disposed of by landfill burial. The alkalinity of peat ash alters the soil quality of the landfill site 43 44 such that only alkali tolerant plants can grow during the years immediately after disposal. The 45 composition of peat ash varies with location but typically contains a mixture of silicon-, aluminium-, calcium- and iron-containing species, and a range of toxic elements including 46 arsenic and cadmium [7-10]. While its elemental composition has been well studied, a 47 48 definitive characterisation of peat ash mineralogy is lacking in the literature. The few papers that discuss peat ash infer crystal phases from (a) elemental composition by scanning electron 49 microscopy/energy-dispersive X-ray spectroscopy (SEM/EDAX) or X-ray fluorescence (XRF) 50

only and/or (b) unseen XRD data; the reader is thus advised to treat such assertions with
caution. For example, quartz, microcline, albite and calcium sulfate were reported to be present
in peat ash samples, although no XRD results were shown [7, 8].

The transformation of peat ash to a useful value-added product with industrial applications 54 would be a significant improvement on the current method of disposal. One such possibility is 55 to use peat ash to prepare zeolites, which are high surface area aluminosilicates widely used 56 for water treatment and purification, humidity control, and heterogeneous catalysis [11]. The 57 combustion of fossil fuels and biomass produces ash residue that contains silicon and 58 59 aluminium based minerals in appropriate quantities to those used to prepare aluminosilicate zeolites. Coal fly ash has been extensively studied as a zeolite synthesis reagent, and a variety 60 of zeolite architectures were successfully prepared using the alkali fusion method [12-23]. 61 62 More recently, there are reports showing zeolite preparation using ash from the following renewable biomass sources: rice husk [24-27] eucalyptus bark residue [28], pulp from paper 63 industry [29], sawdust and pine bark [30], bamboo [31] and cogon grass [32]. 64

We now report the mineralogy of peat ash and its successful transformation to pure zeolite using a single stage purification step. To our knowledge, this is the first report of zeolite prepared using peat ash. The zeolites formed removed heavy metals from aqueous solution with practically similar quantities to those of a reference zeolite.

69

### 70 2. Materials and Methods

#### 71 2.1 Materials

Peat ash, from Ireland, was collected and combusted as follows: (a) sample A (lime added), *Bord na Móna ltd.*, industrial boiler (b) sample B, air-dried peat sods from county Roscommon,
domestic stove. The following is a list of the materials' source/supplier and purity; hydrochloric
acid (HCl), concentration >37%, Fluka; nitric acid 70% w/w; sodium hydroxide (NaOH)

pellets (anhydrous), extra pure, Sigma-Aldrich; sodium aluminate (NaAlO<sub>2</sub>), general purpose,
Fischer; sodium silicate solution, general purpose, Merck. Copper(II) nitrate trihydrate
Cu(NO<sub>3</sub>)<sub>2</sub>.3H<sub>2</sub>O, cobalt(II) nitrate hexahydrate Co(NO<sub>3</sub>)<sub>2</sub>.6H<sub>2</sub>O, lead nitrate Pb(NO<sub>3</sub>)<sub>2</sub>, zinc
nitrate hexahydrate Zn(NO<sub>3</sub>)<sub>2</sub>.6H<sub>2</sub>O and cadmium nitrate tetrahydrate Cd(NO<sub>3</sub>)<sub>2</sub>.4H<sub>2</sub>O were
all 99.99% purity and supplied by Sigma-Aldrich.

81

## 82 **2.2 Zeolite synthesis**

The samples were calcined in air at 600 °C (sample A) and 800 °C (sample B) for 4 h to remove 83 organic matter. Acid extraction was conducted by treating 30 g of calcined peat ash in 500 cm<sup>3</sup> 84 acid for 5 h as follows: Sample A was stirred in 5 M HNO<sub>3</sub> at room temperature, and sample 85 B was refluxed in 5 M HCl at 95 °C. The product was recovered by filtration and dried at 80 86 87 °C. Unless otherwise stated, 1 part of the acid extracted ash was ground in a mortar and pestle with 2.4 parts (by mass) NaOH, heated at 600 °C in air for 3 h in a furnace, and crushed to 88 powder form after cooling to ambient temperature. 1 part alkali fused ash was then added to 10 89 90 parts water in a polypropylene bottle, stirred at room temperature for 3 days, and hydrothermally treated at 90 °C for 24 h. Sodium aluminate was added prior to alkali fusion to 91 give Si/Al ratios (of synthesis reagents) of 5 and 1 to produce GIS and LTA, respectively. 92 Additional ageing of the Si/Al ratio 1 suspension was done for 4 days at 35 °C to produce FAU. 93 Products were recovered by filtration and calcined in air at 550 °C for 4 h using a ramp rate of 94 5 °C min<sup>-1</sup>. A reference FAU zeolite was prepared from a synthesis solution with the molar 95 composition  $8NaOH : 0.2Al_2O_3 : 1.0SiO_2 : 200H_2O$  [33]. The hydrothermal treatment was 96 performed at 80 °C for 24 h. 97

98

## 99 2.3 Characterisation

100 XRD was conducted in ambient conditions using a Panalytical X'Pert Powder diffractometer with Cu K $\alpha$  radiation ( $\lambda = 1.5406$  Å). All powder diffraction patterns were recorded from 4 to 101  $120^{\circ} 2\theta$  with step size 0.013 ° and step time 50 s, using an X-ray tube operated at 40 kV and 102 30 mA with fixed 1/4 ° anti-scatter slit. A Rigaku NEX-CG (XRF) spectrometer was used for 103 analysis using the loose powder method under vacuum. Nitrogen 104 elemental adsorption/desorption measurements were carried out using a Micromeritics ASAP 2020 105 surface area analyser at -196 °C. Samples were degassed under vacuum ( $p < 10^{-5}$  mbar) for 5 106 h at 200 °C prior to analysis. Brunauer-Emmett-Teller (BET) surface areas of the samples 107 were calculated in the relative pressure range 0.05-0.30. Microscopic images were recorded 108 using a JEOL JSM-5600LV SEM. 109

110

## 111 **2.4 Adsorption study**

112 Cu(NO<sub>3</sub>)<sub>2</sub>.3H<sub>2</sub>O, Co(NO<sub>3</sub>)<sub>2</sub>.6H<sub>2</sub>O, Pb(NO<sub>3</sub>)<sub>2</sub>, Zn(NO<sub>3</sub>)<sub>2</sub>.6H<sub>2</sub>O and Cd(NO<sub>3</sub>)<sub>2</sub>.4H<sub>2</sub>O were 113 dissolved together in water and diluted to give a solution that was 100 ppm in each of Cu, Co, 114 Pd, Zn and Cd. 20 cm<sup>3</sup> of this solution were added to 0.1 g LTA (sample A), stirred at 180 rpm 115 for 1 h at room temperature and the solid removed by filtration. The concentrations of metals 116 before and after adsorption were determined using a Thermo Scientific iCAP 6000 Series 117 inductively coupled plasma-optical emissions spectrometer (ICP-OES).

118

#### 119 **3. Results and Discussion**

# 120 **3.1** Crystallography and elemental composition

SEM images, Fig. 1, show that both raw and calcined peat ash lack any regular morphology, which is in contrast to the spherically shaped particles routinely observed for coal fly ash [12]. Results also showed that calcination did not cause an observable transformation in particle morphology. Phase identification, performed by matching the XRD peak positions in Fig. 2 125 against the Crystallography Open Database, confirms that the major phases detected for sample A are anhydrite (CaSO<sub>4</sub>), quartz (SiO<sub>2</sub>), calcite (CaCO<sub>3</sub>), lime (CaO) and merwinite 126 (Ca<sub>3</sub>Mg(SiO<sub>4</sub>)<sub>2</sub>). Sample B contains anhydrite, quartz and magnetite (Fe<sub>3</sub>O<sub>4</sub>). A quantitative 127 128 elemental analysis using XRF, Table 1, shows the 10 most concentrated elements present (for sample A) and confirms that the major 'impurities' (in terms of zeolite synthesis) are Ca and 129 Fe based species. The major element present in Sample A is Ca at 53.9 wt% (as oxide) in 130 agreement with the XRD analysis (Fig. 2). Sample B contains 21.2 wt% CaO and 22.0 wt% 131 Fe<sub>2</sub>O<sub>3</sub>. The greater quantity of CaO in sample A is due to the addition of lime to commercial 132 133 peat to reduce SO<sub>x</sub> emissions, which may have reacted to produce anhydrite. It is interesting then that sample B, which has not been treated with lime, also contains anhydrite. 134

135

136

137

138

\_\_\_\_

139

140

Fig. 1. Typical SEM images of peat ash: (a) raw and (b) calcined.

1 µm

11 µµm



141

Fig. 2. XRD powder patterns of calcined peat ash.

It is not possible to make a meaningful comparison of the XRD results presented here with published data on peat ash mineralogy, as such reports contain insufficient results [7,8]. However, all such studies confirm that the main elements present in peat ash are Ca, Fe, Si and Al, which correlates well with our XRD and XRF results.

143

149

Table 1: XRF elemental composition of peat ash in wt% following calcination and acid extraction.

	Α		В	
	Calcined	Acid extracted	Calcined	Acid extracted
CaO	53.9	0.81	21.2	0.77
SiO <sub>2</sub>	9.47	71.4	12.7	76.9
$SO_3$	7.32	0.58	22.4	0.26
$Fe_2O_3$	4.81	1.29	22.0	0.61
MgO	2.20	0.12	10.4	0.35
Al <sub>2</sub> O <sub>3</sub>	1.63	2.55	6.58	3.77
MnO	0.35	0.03	0.30	0.02
$P_2O_5$	0.26	0.05	1.87	0.05
K <sub>2</sub> O	0.19	0.97	0.97	1.12
TiO <sub>2</sub>	0.15	0.50	0.45	0.90

150

151 Dissolution by acid extraction considerably reduced the quantities of Ca and Fe in both samples. The Si/Al ratios of acid extracted peat ashes are 28.0 for sample A and 20.4 for sample 152 B. XRD patterns confirm that acid extraction removes all detectable non-quartz crystalline 153 phases, Fig. 3. The majority of zeolite preparations using coal ash do not remove impurities by 154 acid extraction, so it is not surprising that a greater ratio of NaOH to ash is required for the peat 155 156 ash samples explored here to achieve full quartz decomposition due to the higher quantity of quartz [12]. Fig. 3 shows that the mass ratio of 1.2:1 NaOH to ash (chosen as a starting point 157 based on reference [22]) was insufficient but that higher ratios removed quartz completely; a 158 mass ratio of 2.4:1 was used in all further preparations. The other peaks in Fig. 3 confirm the 159 presence of silicates and aluminosilicates, as reported in the literature [34]. 160



Fig. 3. XRD patterns of sample A after acid leaching and the acid-leached sample after alkali fusion at
 600 °C using different sample:NaOH mass ratios as indicated on the figure; the asterisks indicate
 quartz peaks.

165

## 166 **3.2 Zeolite formation**

167 The XRD patterns in Figs. 4 and 5 confirm that peat ash was transformed to zeolite frameworks GIS, LTA and FAU through changes in the synthesis parameters viz. addition of sodium 168 aluminate for LTA, and extended ageing time for FAU. Non-zeolitic crystalline phases were 169 not observed by XRD in any detectable quantities. The effect of altering the Si/Al ratio by 170 adding external silica was found to alter the crystal phase produced in a study of the 171 crystallisation mechanism of zeolite from coal fly ash, where FAU was not formed until the 172 Si/Al ratio was reduced to approximately 1.5 [35]. SEM images, Fig. 6, show the morphology 173 of GIS, the characteristic cubic ca. 1 µm sized particles of LTA and the sub-micron 174 175 agglomerated FAU particle morphology, providing further evidence of the presence of these phases. The Si/Al ratios are shown in Table 2: the Si/Al ratios of FAU are 1.32 and 1.35, so 176 these samples are zeolite X. The highest BET surface areas were recorded for the FAU 177 structures, which were calculated to be 486 and 319 m<sup>2</sup> g<sup>-1</sup>. 178





Fig. 4 XRD patterns of zeolites prepared using sample A.



Fig. 5 XRD patterns of zeolites prepared using sample B.

Table 2: BET surface areas and Si/Al elemental ratios.

	Surface area (m <sup>2</sup> g <sup>-1</sup> )		Si/Al	
	Α	В	Α	В
Raw	24	25	4.04	1.55
Calcined	6	22	4.94	1.64
FAU	486	319	1.32	1.35
LTA	84	55	1.41	1.35
GIS	77	104	2.83	2.83



196

Fig. 6. Typical SEM images of different zeolites types prepared from peat ash.

The characteristics of zeolites prepared from peat ash also compare well with analogous studies 198 using fly ash. For example, the highest surface area reported by Tosheva et al. for FAU 199 prepared from fly ash was 441 m<sup>2</sup> g<sup>-1</sup>, relative to 486 m<sup>2</sup> g<sup>-1</sup> for that prepared here [23]. The 200 classification of coal is based on the relative amounts of organic and inorganic materials, age, 201 and quantity of heat energy that can be produced. Most reports in the literature describing coal 202 203 ash to zeolite conversions are for sub-bituminous (up to 45% carbon) bituminous (86%) and 204 anthracitic (97%) coal types. Lignite has lower carbon content than sub-bituminous coal and, because it is formed over time from compressed peat, which has carbon content less than 40-205 55%, seems the most appropriate comparison to the results presented here [1-3]. Kunecki et al. 206 used lignite, containing quartz, anhydrite and gehlenite, to prepare zeolite [36]. Both LTA and 207 FAU frameworks were prepared by varying experimental conditions, but not in pure form. The 208 highest BET surface area for FAU was 256 m<sup>2</sup> g<sup>-1</sup>, which was significantly lower than the FAU 209

from either sample in this study, 486 and 319 m<sup>2</sup> g<sup>-1</sup>. The increased crystal purity and surface 210 area for zeolite prepared using peat ash is tentatively attributed to the removal of impurities in 211 the starting material by acid extraction. Anhydrite is highly soluble in aqueous solution and its 212 presence during zeolite crystallisation, as in the case of lignite to zeolite, reduces the solubility 213 of silicates and aluminosilicates, which will negatively impact both the formation of zeolite 214 nuclei and the subsequent dissolution and crystallisation of zeolite during hydrothermal 215 treatment. Furthermore, ions in solution are known to interact with zeolite frameworks during 216 crystallisation, so the  $Ca^{2+}$  and  $SO_4^{2-}$  ions from anhydrite may have a negative effect on the 217 218 formation of zeolite [37].

219

## 220 **3.3 Adsorption study**

221 The prepared zeolites were tested as adsorbents in the removal of heavy metals lead, cadmium, cobalt, zinc and copper from aqueous solution; these metals were chosen on the basis of their 222 toxicity and presence in wastewater streams [38]. The results, Fig. 7, showed that all zeolites 223 actively removed the range of metals between 10 and 60 minutes, in which the quantities of 224 lead, cadmium, zinc and copper adsorbed using peat ash prepared zeolites were slightly higher 225 than those measured for the FAU- reference. In the case of cobalt, adsorption was higher using 226 FAU-type zeolites than LTA-, while the most active adsorbent was that prepared from sample 227 A, which showed near identical properties to that of the reference zeolite. A more in-depth 228 229 study of metals adsorption on zeolites viz. influence of concentration, temperature, and kinetics is currently underway and will be published as a follow up to this paper. While the focus of 230 this paper is the preparation of pure zeolite from peat ash, the adsorption results are included 231 232 to validate the efficacy of such materials in real applications.











Fig. 7. Metal removal (as % of original concentration) of (a) lead (b) cadmium (c) cobalt (d) zinc and
(e) copper on LTA- and FAU-type zeolites prepared from peat ash and an FAU- reference.

240

## 241 4. Conclusions

Zeolites were successfully prepared from peat ash using a combination of acid leaching, alkali
fusion and hydrothermal treatment. The framework structure was systematically varied such
that crystal phases of GIS, LTA and FAU-type zeolites were each prepared. The prepared
zeolites were active in the removal of a range of metals from aqueous solution.

246

# 247 Acknowledgments:

The authors thank; Patrick Bowens, Co. Roscommon, and Imelda Egan and Colman Hynes,
Bord na Móna, for supplying peat ash; Dr Paul Bolger, University College Cork, for arranging
the link with Bord na Móna. Ifeoma V Joseph is grateful to the Schlumberger Foundation for
funding a PhD studentship; Giulia Roncaglia is grateful to Erasmus+ and Manchester
Metropolitan University for financial assistance.

- 253
- 254

#### 255 References

- 256 1. F. Parish, A.A. Sirin, D. Charman, H. Joosten, T. Minayeva, M. Silvius, Assessment on
- 257 Peatlands, Biodiversity and Climate Change: Executive Summary. Global Environmental
- 258 Centre, Malaysia and Wetlands International, Wageningen, The Netherlands, 2007.
- 259 2. E. Lappalainen, Global Peat Resources, The International Peat Society, Finland 1996.
- 260 3. World Energy Council Report, World Energy Resources 2013 Survey: Peat.
- 261 4. Department of Agriculture, Food and the Marine Ireland, Rural Development Programme
- 262 2014a.
- 5. Sustainable Energy Authority of Ireland 2017 Report, Energy in Ireland 1990-2016.
- 264 6. Eirgrid Group, All-Island Generation Capacity Statement 2017-2026.
- 265 7. J. Fagerström, I.-L. Näzelius, C. Gilbe, D. Boström, M. Öhman, C. Boman, Influence of peat
- ash composition on particle emissions and slag formation in biomass grate co-combustion,
  Energy Fuels 28 (2014) 3403-3411. https://dx.doi.org/10.1021/ef4023543.
- 8. L. Pommer, M. Öhman, D. Boström, J. Burvall, R. Backman, I. Olofsson, A. Nordin,
  Mechanisms behind the positive effects on bed agglomeration and deposit formation
  combusting forest residue with peat additives in fluidized beds, Energy Fuels 23 (2009) 42454253. https://doi.org/10.1021/ef900146e.
- 9. B-M. Steenari, O. Lindqvist, Fly ash characteristics in co-combustion of wood with coal, oil
  or peat, Fuel 78 (1999) 479-488. https://doi.org/10.1016/S0016-2361(98)00177-X.
- 10. S.V. Vassilev, D. Baxter, L.K. Andersen, C.G. Vassileva, An overview of the composition
  and application of biomass ash. Part 1. Phase–mineral and chemical composition and
  classification, Fuel 10 (2013) 40-76. https://doi.org/10.1016/j.fuel.2012.09.041.
- 277 11. J. Weitkamp, Zeolites and catalysis, Solid State Ionics 131 (2000) 175-188.
  278 https://doi.org/10.1016/S0167-2738(00)00632-9.
- 12. C. Belviso, State-of-the-art applications of fly ash from coal and biomass: A focus on
  zeolite synthesis processes and issues, Prog. Energy Combust. Sci. 65 (2018) 109-135.
  https://doi.org/10.1016/j.pecs.2017.10.004.
- 13. X. Querol, N. Moreno, J.C. Umaña, A. Alastuey, E. Hernández, A. López-Soler, F. Plana,
- Synthesis of zeolites from coal fly ash: an overview. Int. J. Coal Geol. 50 (2002) 413-423.
  https://doi.org/10.1016/S0166-5162(02)00124-6.
- 285 14. X. Querol, J.C. Umaña, F. Plana, A. Alastuey, A. López-Soler, A. Medinaceli, A. Valero,
- 286 M.J. Domingo, E. Garcia-Rojo. Synthesis of Na zeolites from fly ash in a pilot plant
- scale. Examples of potential environmental applications, Fuel 80 (2001) 857-865.

- 15. N. Murayama H. Yamamoto J. Shibata, Mechanism of zeolite synthesis from coal fly ash
  by alkali hydrothermal reaction. Int. J. Miner. Process. 64 (2002) 1-17.
  https://doi.org/10.1016/S0301-7516(01)00046-1.
- 16. H. Tanaka, S. Matsumura, R. Hino, Formation process of Na-X zeolites from coal fly ash.
- 292 J. Mater. Sci. 39 (2004) 1677-1682. https://doi.org/10.1023/B:JMSC.0000016169.85449.86.
- 17. T.T. Wałek, F. Saito, Q. Zhang, The effect of low solid/liquid ratio on hydrothermal
  synthesis of zeolites from fly ash. Fuel 87 (2008) 3194-3199.
  https://doi.org/10.1016/j.fuel.2008.06.006.
- 18. H. Tanaka, A. Fujii. Effect of stirring on the dissolution of coal fly ash and synthesis of
- 297 pure-form Na-A and -X zeolites by two-step process, Adv. Powder Technol. 20 (2009) 473298 479. https://10.1016/j.apt.2009.05.004
- 19. M. Gross-Lorgouilloux, P. Gaullet, M. Soulard, J. Patarin, E. Moleiro, I. Saude, Conversion
- 300 of coal fly ashes into faujasite under soft temperature and pressure conditions. Mechanisms of
- 301 crystallisation, Microporous Mesoporous Mater. 131 (2010) 407-417.
- 302 https://doi.org/10.1016/j.micromeso.2010.01.022.
- 20. N. Shigemoto, H. Hayashi, K. Miyaura, Selective formation of Na-X zeolite from coal fly
  ash by fusion with sodium hydroxide prior to hydrothermal reaction, J. Mater. Sci. 28 (1992)
  4781-4786. https://doi.org/10.1007/BF00414272.
- 306 21. H.-L. Chang, W.-H. Shih, A general method for the conversion of fly ash into zeolites as
- 307 ion exchangers for cesium, Ind. Eng. Chem. Res. 37 (1998) 71-78. https://10.1021/ie970362o.
- 308 22. A. Molina, C. Poole, A comparative study using two methods to produce zeolites from fly
- ash, Miner. Eng. 17 (2004) 167-173. https://doi.org/10.1016/j.mineng.2003.10.025.
- 310 23. L. Tosheva, A. Brockbank, B. Mihailova, J. Sutula, J. Ludwig, H. Potgieter, J. Verran,
- 311 Micron- and nanosized FAU-type zeolites from fly ash for antibacterial applications, J. Mater.
- 312 Chem. 22 (2012) 16897-16905. https://10.1039/C2JM33180B.
- 24. D. Prasetyoko, Z. Ramli, S. Endud, H. Hamdan, B. Sulikowski, Conversion of rice husk
  ash to zeolite beta, Waste Management, 26 (2006) 1173-1179.
  https://doi.org/10.1016/j.wasman.2005.09.009.
- 25. R.K. Vempati, R. Borade, R.S. Hegde, S. Komarneni, Template free ZSM-5 from siliceous
- rice hull ash with varying C contents, Microporous Mesoporous Mater. 93 (2006) 134-140.
- 318 https://doi.org/10.1016/j.micromeso.2006.02.008.
- 26. E.-P. Ng, H. Awala, K.-H. Tan, F. Adam, R.d Retoux, S. Mintova, EMT-type zeolite
- 320 nanocrystals synthesized from rice husk, Microporous Mesoporous Mater. 204 (2015) 204-
- 321 209. https://doi.org/10.1016/j.micromeso.2014.11.017.

- 27. Jia-Tian Wong, Eng-Poh Ng, Farook Adam, Microscopic investigation of nanocrystalline
  zeolite L synthesized from rice husk ash, J. Am. Ceram. Soc. 95 (2012) 805–808.
  https://doi.org/10.1111/j.1551-2916.2011.04995.x.
- 28. I. Jiménez, G. Pérez, A. Guerrero, B. Ruiz, Mineral phases synthesized by hydrothermal 325 326 from biomass ashes, Int. J. Miner. Process. 158 (2017)8-12. treatment https://doi.org/10.1016/j.minpro.2016.11.002. 327
- 328 29. S. Vichaphund, D. Aht-Ong, V. Sricharoenchaikul, D. Atong, Characteristic of fly ash
- 329 derived-zeolite and its catalytic performance for fast pyrolysis of Jatropha waste, Environ.
- 330 Technol. 35 (2014) 2254-61. https://doi.org/10.1080/09593330.2014.900118.
- 30. T. Fukasawa, A. Horigome, T. Tsu, A.D. Karisma, N. Maeda, A.-N. Huang, K. Fukui,
- Utilization of incineration fly ash from biomass power plants for zeolite synthesis from coal
  fly ash by hydrothermal treatment, Fuel Process. Technol. 167 (2017) 92–98.
  https://doi.org/10.1016/j.fuproc.2017.06.023.
- 31. E.-P. Ng, J.-H. Chow, R.R. Mukti, O. Muraza, T.C. Ling, K.-L. Wong, Hydrothermal
  synthesis of zeolite A from bamboo leaf biomass and its catalytic activity in cyanoethylation
  of methanol under autogenic pressure and air conditions, Mater. Chem. Phys. 201 (2017) 7885. https://doi.org/10.1016/j.matchemphys.2017.08.044.
- 339 32. K. Bunmai, N. Osakoo, K. Deekamwong, W. Rongchapo, C. Keawkumay, N. Chanlek, S.
- 340 Prayoonpokarach, J. Wittayakun, Extraction of silica from cogon grass and utilization for
- 341 synthesis of zeolite NaY by conventional and microwave-assisted hydrothermal methods, J.
- 342 Taiwan Inst. Chem. E. 83 (2018) 152–158. https://doi.org/10.1016/j.jtice.2017.11.024.
- 343 33. V. P. Valtchev, K. N. Bozhilov, Transmission electron microscopy study of the formation
  of FAU-type zeolite at room temperature, J. Phys. Chem. B 108 (2004) 15587-15598.
  https://pubs.acs.org/doi/abs/10.1021/jp048341c.
- 34. A.M. Doyle, Z.T. Alismaeel, T.M. Albayati, A.S. Abbas, High purity FAU-type zeolite
  catalysts from shale rock for biodiesel production, Fuel 199 (2017) 394-402.
  https://doi.org/10.1016/j.fuel.2017.02.098.
- 349 35. M. Gross-Lorgouilloux, P. Caullet, M. Soulard, J. Patarin, E. Moleiro, I. Saude, Conversion
  of coal fly ashes into faujasite under soft temperature and pressure conditions. Mechanisms of
  351 crystallisation, Microporous and Mesoporous Materials 131 (2010) 407–417.
- 352 https://doi.org/10.1016/j.micromeso.2010.01.022.
- 353

- 354 36. P. Kunecki, R. Panek, M. Wdowin, W. Franus, Synthesis of faujasite (FAU) and
- tschernichite (LTA) type zeolites as a potential direction of the development of lime Class C
- 356 fly ash, Int. J. Miner. Process. 166 (2017) 69-78. https://doi.org/10.1016/j.minpro.2017.07.007.
- 357 37. R.M. Shayib, N.C. George, R. Seshadri, A.W. Burton, S.I. Zones, B. F. Chmelka, Structure-
- 358 directing roles and interactions of fluoride and organocations with siliceous zeolite
- 359 frameworks, J. Am. Chem. Soc. 133 (2011) 18728–18741. https://10.1021/ja205164u.
- 360 38. F. Fenglian, Q. Wang, Removal of heavy metal ions from wastewaters: A review, J.
- 361 Environ. Manage. 92 (2011) 407-418. https://doi.org/10.1016/j.jenvman.2010.11.011.