

1 **The effect of extrusion screw-speed on the water extractability and molecular**
2 **weight distribution of arabinoxylans from defatted rice bran**

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24 **Abstract**

25 Arabinoxylans (AXs) are major dietary fibre in cereals. Recently, AXs have attracted
26 a great deal of attention because of their biological activities. These activities have
27 been suggested to be related to the content of low molecular weight (Mw) AXs, in
28 particular those with a Mw below 32 kDa.

29 Rice bran is a rich source of AXs. However, water extraction of AXs is difficult and
30 often gives low yield. Extrusion processing has been used to increase the solubility of
31 cereal dietary fibre. The aim of this research was to study the effect of extrusion screw-
32 speeds of 80 and 160 rpm on the extraction yield and Mw of water extractable AXs
33 from rice bran. It was found that the extraction yield of AXs increased significantly
34 ($P<0.05$) with an increase in screw speed and was accompanied by a significant
35 decrease ($P<0.05$) in the Mw of AXs from extruded rice bran.

36 **Keywords**

- 37 • Rice bran, dietary fibre, water soluble arabinoxylans, extrusion technology,
38 low molecular weight

39

40 **Introduction**

41 Extrusion cooking is an important food processing technology, especially for the
42 production of cereal-based products (Vasanthan et al. 2002). It involves the cooking
43 of expansive, moistened food materials in a tube by the application of high
44 temperature, high shear forces and high pressure for a short time and results in
45 structural modification by physiochemical changes and molecular re-distribution
46 (Pawar et al. 2014; Thymi et al. 2005).

47 Several researchers have investigated the effects of extrusion on the composition of
48 cereal-based products. Vasanthan et al. (2002) reported that extrusion could increase
49 the soluble dietary fibre (SDF) in extruded barley flour. The increase of SDF content
50 was from 5.62% in non-extruded barley flour to 7.24% in extruded barley flour under
51 a barrel temperature of 140°C, screw-speed of 50 rpm and moisture content of 50%.
52 The increase in SDF was explained by transglycosylation from non-dietary fibre
53 components (i.e. starch) to SDF and transformation of insoluble dietary fibre (IDF) to
54 SDF.

55 Recently, Daou and Zhang (2012) investigated the effect of extrusion cooking on rice
56 bran dietary fibre solubility. A twin-screw extruder was used with a screw-speed of 90
57 rpm. They found that the content of soluble fibre increased from 5.9% in non-extruded
58 samples to 6.8% in extruded samples, and concluded the increase in dietary fibre
59 solubility may be due to the reduction in particle sizes of extruded samples. Another
60 possible explanation for the increase in dietary fibre solubility may be the breakdown
61 of covalent and non-covalent bonds in larger molecules due to the high temperature
62 of the barrel (Rashid et al. 2015). Gualberto et al. (1997) showed a significant decrease
63 in IDF in extruded dietary fibre of rice, oats and wheat but a significant increase in SDF
64 in all samples.

72 Arabinoxylans (AXs) are major dietary fibres found in many cereals such as wheat and
73 rice (Broekaert et al. 2011). Few researchers have investigated the effect of extrusion
74 cooking on the solubility and molecular weight distribution of AXs. Santala et al. (2013)
75 investigated the effect of extrusion cooking on water extractable arabinoxylan (WEAX)
76 levels and molecular weight obtained from wheat bran. The extrusion of wheat bran
77 increased the solubility of AXs from 1.7% to 2.5% when the water content decreased
78 from 92% to 42-60% respectively under a fixed screw-speed at 65 rpm and fixed barrel
79 temperature of 50 °C. Optimal WEAX levels and significantly lower Mw WEAX were
80 obtained from extruded wheat bran at a water content of 48-60%.

81 The aim of this study was to determine the effect of extrusion on solubility and
82 molecular weight distribution of AXs from rice bran. It has been reported that low
83 molecular weight (30-50 kDa) AXs have immunomodulatory effects, both *in vivo* and
84 *in vitro* (Ghoneum and Matsuura 2004). Our hypothesis is that lower molecular weight
85 AXs would be observed through extrusion than with water extraction alone, thus
86 highlighting extrusion as a valuable method to enrich AXs with most potential health
87 benefits from cereals.

88 **Materials and methods**

89 **Rice bran and chemicals**

90 Ener-G, General Dietary Ltd (Surrey, UK) kindly provided rice bran. D-(+)-Xylose,
91 dextrose (D-glucose) anhydrous, acetic acid (glacial), hydrochloric acid, phloroglucinol
92 and ethanol were purchased from Sigma-Aldrich (Brøndby, Denmark) for the
93 determination of xylose in rice bran. Eight pullulan (linear α -(1-4) glucans with no side
94 chain) standards of varying molecular weights (ranging from 5-708 kDa) were
95 purchased from Shodex (Shanghai, China) to characterise the Mw of AXs by SEC-

96 HPLC. Sodium nitrate (NaNO_3) and sodium, azide (NaN_3) were purchased from
97 Sigma-Aldrich (Gillingham, UK) for the HPLC mobile phase.

98 **Enzymes**

99 Termamyl (α -amylase), type XII-A, A3403-1MU and proteinase, type XXIII, P4032
100 were purchased from Sigma-Aldrich (Brøndby, Denmark).

101 **Fat extraction**

102 Rice bran fats were extracted prior to extrusion using the method provided by Buchi
103 (2016). Briefly, 10 g of rice bran was mixed with 40 ml of petroleum ether (Fisher
104 Scientific, Loughborough) and transferring to an E-812/E-816 HE extraction unit
105 (Buchi, Switzerland).

106 **Extrusion pre-treatment**

107 A Werner Pfleiderer Continua 37 co-rotating, self-wiping twin-screw extruder (Werner
108 Pfleiderer, Stuttgart, Germany) was used for the extrusion pre-treatment of rice bran.
109 The extruder had the following characteristics: a length to diameter ratio (L/D) of 27:1,
110 screw-speeds (SS) of 80 rpm and 160 revolution per minute (rpm) and a feed rate of
111 10 kg/h. The barrel temperature was set at 80 to 140°C (feed end and die end
112 respectively) with a fixed moisture content of 30% (w/w wet weight basis). Extruded
113 samples were dried at 60°C for 12 hours.

114 **Extraction of water-extractable AXs (WEAXs)**

115 Li et al. (2013) method was used to extract the WEAXs. Rice bran samples (100 g)
116 were extracted with 333 ml water, incubating in a shaking water bath (Precision SWB
117 15, ThermoScientific, London, UK) for two hours at 40°C. Samples were then
118 centrifuged for 40 minutes at 6000 x g and supernatants transferred to Erlenmeyer
119 flasks with pH adjusted to pH7 using (1M HCl) or (1M NaOH) before adding 400 ppm

120 thermostable α -amylase (500 Units/mg) and incubating in a water bath at 91°C for 60
121 minutes. Samples were then cooled to room temperature and before removing protein
122 with the addition of 400 ppm proteinase (3 Units/mg) at 50°C for 14h. The proteinase
123 was then deactivated by placing samples in a boiling water bath for 10 minutes.
124 Samples were allowed to cool to room temperature and centrifuged at 4600 x g for 20
125 minutes. Ethanol (70:30 v/v in distilled water) was added to supernatants at 4°C
126 overnight. The precipitate that formed was recovered by centrifugation at 4600 x g for
127 20 minutes, discarding supernatant and retaining the residue. The residue was
128 weighed before washing and vortexing twice with 20 ml absolute ethanol (minimum
129 99%). Finally, 20ml acetone was added and samples vortexed for one minute followed
130 by centrifugation at 4600 x g for 20 minutes. The final precipitates were dried for 48
131 hours at 45°C in a drying oven before transferring to vacuum-sealed, food-grade bags
132 using a Turbovac SB425 Vacuum Packer (Stockport, UK) and storing at 21°C until
133 further analysis.

134 **Water-extractable arabinoxylan (WEAX) determination**

135 The percentage of xylose in extracts was determined using a phloroglucinol assay
136 following the method described by Douglas (Douglas 1981). The absorbance of each
137 sample was measured at 552 nm and 510 nm using a ThermoScientific GENESYS
138 10S Bio Spectrophotometer (London, UK). A xylose standard curve was constructed
139 to determine the xylose content of rice bran samples, which was subsequently used
140 to calculate the amount of AXs in rice bran extracts.

141 **Determination of sugar composition of purified extracts by HPLC**

142 The sugar composition of purified extracts was determined using a method adapted
143 from Zheng et al. (2011). A Shimadzu LC-20 AB HPLC system, (Shimadzu

144 Corporation, Tokyo, Japan), equipped with a Refractive Index Detector (RID) 10A,
145 SUPELGuard Pb (5 cm × 4.6 mm) guard column (Phenomenex, Macclesfield, UK)
146 and SUPELCOGEL Pb (30 cm × 7.8 mm) column (Ion exclusion separation mode)
147 (Phenomenex, Macclesfield, UK) was used to determine the sugar content of samples.
148 The column temperature, mobile phase and flow rate were 80°C, HPLC grade water
149 and 0.5 ml/min respectively in an isocratic run. Different concentrations (0.25, 0.5, 0.75
150 and 1 mg/ml) of glucose, xylose, galactose and arabinose were prepared as standards
151 to plot a series of calibration curves from which the amount of each sugar was
152 calculated based upon the relative peak areas.

153 **Molecular weight standard curve**

154 Five pullulan standards ranging from 5-375 kDa were used to construct the standard
155 curve. Standards were prepared at 0.5 mg/ml using mobile phase and left overnight
156 at 5°C. All samples and standards were filtered through a 0.45 µm nylon membrane
157 and transferred to 1 ml glass shell vials. To prepare the pullulan standard curve, the
158 pullulan molecular weights were converted to log molecular weights before plotting
159 against the retention time.

160 **Determination of the molecular weight distribution of AXs by HPLC**

161 Dry samples were prepared for analysis by dissolving 2 mg of each sample in 1 ml
162 mobile phase and leaving overnight at 5°C. The mobile phase was prepared by
163 dissolving 0.65 g NaN₃ and 17g NaNO₃ in 2000 ml HPLC-grade water.

164 The molecular weight distribution of AXs was determined using size exclusion
165 chromatography. All samples were analysed using a Shimadzu LC-10 HPLC
166 (Shimadzu Corporation, Kyoto, Japan) equipped with a JASCO RI-2031 Refractive
167 Index (RI) Detector (Jasco Corporation, Tokyo, Japan), and BioSep-SEC-S 4000 and

168 BioSep-SEC-S 3000 columns (Phenomenex, Macclesfield, UK). An isocratic run was
169 used, with a flow rate of 0.6 ml/min (Li et al. 2013).

170 **Statistics**

171 Data were expressed as mean \pm standard error of the mean (SEM). Significant
172 differences between samples were determined by one-way analysis of variance
173 ANOVA. A *P* value < 0.05 was considered statistically significant.

174 **Results**

175 **The effect of extrusion on extraction of AXs from rice bran**

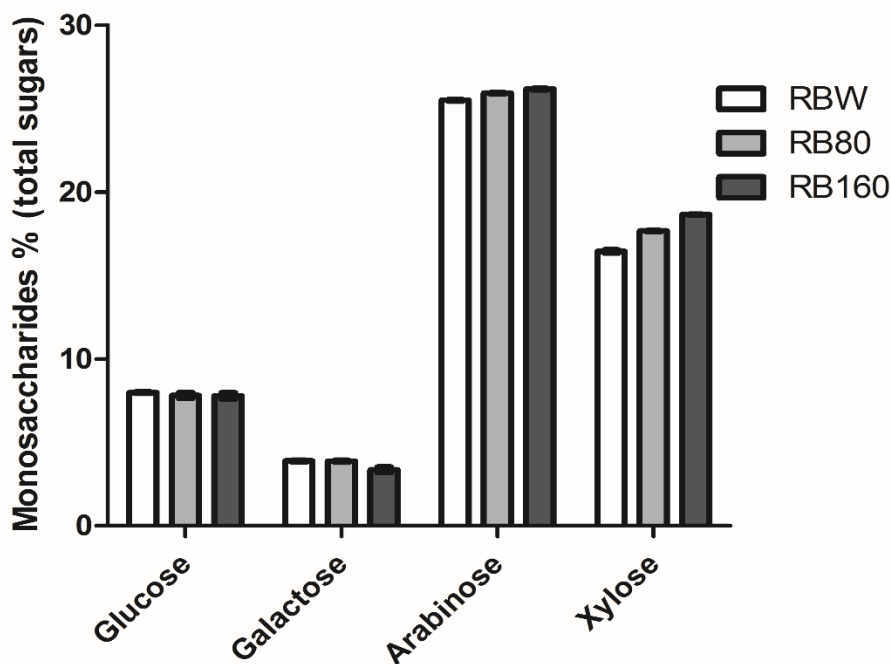
176 The extrusion process had a positive effect on the extraction yield of AXs. An increase
177 in extrusion screw-speed resulted in a significant increase in extraction yield. Total
178 AXs present in samples were calculated using the xylose standard curve and the Ar/Xy
179 ratio obtained by HPLC. Extrusion significantly ($P < 0.05$) increased the percentage of
180 water-extractable AX, from 0.58 % without extrusion to 1.22 % with an extrusion
181 screw-speed of 80 rpm and to 1.62 % with an extrusion screw speed of 160 rpm (Table
182 1).

183 **Table 1. Extraction yield of AXs (%) from rice bran (RB) samples extruded**
184 **at different screw-speeds, 80 rpm (RB80) and 160 rpm (RB160)**

Samples	Ar/Xyl	Total AX
RBW	1.55 \pm 0.020	0.58 \pm 0.082
RB80	1.46 \pm 0.008	1.22 \pm 0.09
RB160	1.40 \pm 0.006	1.62 \pm 0.07

185 **The arabinose to xylose ratio (Ar/Xy) of extracts**

186 Glucose, arabinose, galactose and xylose monosaccharides were identified in the
187 purified AXs from rice bran (Figure 1).



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Figure 1. Sugar composition for purified AXs from rice bran (RB) obtained by water extraction alone (RBW) or via extrusion at 80 rpm (RB80) and 160 rpm (RB160).

193

The ratio of arabinose to xylose (Ar/Xy) decreased in rice bran samples as the extrusion screw-speed increased. The Ar/Xy ratio for water extracted AXs from unextruded rice bran was 1.55 ± 0.2 . The Ar/Xy ratios for extruded rice bran samples were 1.47 ± 0.008 and 1.40 ± 0.006 at screw speeds of 80 and 160 rpm respectively.

197

Molecular weight analysis of AXs using HPSEC

198

Pullulan standard curve construction

199

A standard curve was constructed using five pullulan standards (P5, P20, P100, P200 and P400) analysed by HPLC-SEC and used to determine the molecular weight and retention time of AXs in samples. The Mw of the five pullulan standards ranged between 5.9-375 kDa.

202

203 **Molecular weight distribution of AXs**

204 The Mw distribution of AXs from rice bran samples was characterized by HPLC-SEC.

205 Table 2 illustrates the Mw range of AXs and percentage levels obtained.

206 **Table 2. Mw distribution and Levels (%) of AXs extracted from**
 207 **rice bran (RB) by water extraction alone (RBW) or extrusion at 80**
 208 **rpm (RB80) and 160 rpm (RB160)**

209 Data are presented as mean \pm SEM (n = 3). * indicates significant difference
 210 ($P < 0.05$) in levels of AXs compared to the RBW sample.

Areas	Log Mw	Mw range (kDa)	%		
			RB160	RB80	RBW
Area 1	2.90 - 3.2	0.79 - 1.58	18.24 \pm 0.006 *	14.15 \pm 0.08 *	11.42 \pm 0.0057
Area 2	3.2 - 3.5	1.58 - 3.16	11.52 \pm 0.08	16.13 \pm 0.01 *	13.15 \pm 0.01
Area 3	3.5 - 4	3.16 - 10	45.22 \pm 0.73	47.09 \pm 0.68	44.59 \pm 0.76
Area 4	4 - 4.4	10 - 25.11	25.05 \pm 0.027 *	22.63 \pm 0.008 *	30.84 \pm 0.01

211 Most notably, extrusion with a screw speed of 80 rpm (RB80) and 160 rpm (RB160)
 212 resulted in significantly ($P < 0.05$) higher levels (14.15 \pm 0.08 % and 18.24 \pm 0.006 %
 213 respectively) of very low Mw (0.79-1.58 kDa) AXs compared to extraction without
 214 extrusion (RBW).

215

216 **Discussion**

217 **Extraction rate of water-soluble AXs**

218 In rice bran, WEAX is only around 0.9 % of the total AXs (Hashimoto et al. 1987). The
219 low extractability of AXs could be due the large molecular weight of AXs (Saulnier et
220 al. 2007) and to its ferulic acid (FA) contents (0.31-0.56 mg/g) (Michniewicz et al.
221 1990). FA side chains are esterified to some arabinose residues (Snelders et al. 2013),
222 which form covalent/non-covalent bonds with the cell wall materials, thus decreasing
223 the solubility of AXs in water. Jeon *et al.* (2014) stated that using extrusion cooking,
224 as a pre-treatment is an efficient, environmentally friendly and low-cost process to
225 increase the level of water extractable arabinoxylans in corn fibre. The results of this
226 study confirm those of Jeon *et al.* (2014), showing an increase in the WEAX content
227 of extruded rice bran with progressively increasing screw-speed, from 80 to 160 rpm.
228 There was a 1.1-fold and 1.8-fold increase in WEAX content compared to the un-
229 extruded rice bran sample as the extrusion screw-speed increased from 80 to 160 rpm
230 respectively.

231 The increase in WEAX in extruded samples could be due to; the liberation of FA side
232 chains, the softening of lignin and a reduction of MW by high mechanical shear forces.
233 Holguín-Acuña *et al.* (2008) found that FA content increased from 0.2 mg/g in non-
234 extruded maize bran to 2.5 mg/g in extruded maize bran. The increase in FA content
235 might be the reason for the observed increase in solubility of AXs, since more AXs will
236 be in contact with water as FA becomes liberated from side chains. Moreover, the
237 increase in screw-speeds from 80 to 160 rpm may soften lignin (Yoo et al. 2012). AXs
238 act as a glue between lignin and cellulose (Vermaas et al. 2015), therefore a high
239 screw-speed will create high shear stress in the barrel which might soften the lignin

240 (Yoo et al. 2012), leading to greater exposure of AXs to water and a subsequent
241 increase in solubility.

242 **Molecular weight distribution of AXs from extruded/non-extruded rice bran**

243 Molecular weight determinations for whole wheat AXs were reported to be within the
244 ranges 56-65 kDa using gel permeation chromatography (Girhammar and Nair 1992)
245 and 6-600 kDa for wheat endosperm using HPSEC (Li et al. 2013), the differences
246 most likely arising from the type of wheat material used and the methodology applied
247 for Mw determination. In this study, HPSEC was used to show the Mw of AXs from
248 extruded/non-extruded rice-bran samples was between 0.79-25 kDa. Our findings fell
249 within the lower end of the Mw range of AXs (0.6-500 kDa) previously reported from
250 rice bran by Rose et al. (2009), suggesting HPSEC provides low Mw AXs and a
251 narrower Mw range compared to the alkaline-hydrogen peroxide extraction used by
252 Rose et al.

253 Table 2 demonstrates higher percentage levels of low Mw AXs from extruded rice bran
254 samples compared with non-extruded samples. The increases in the percentage
255 levels of low Mw AXs is probably due to the extrusion process, such as high shear
256 forces and high temperatures resulting in depolymerisation of the fibre (Svanberg et
257 al. 1995). It is also possible that extrusion cooking breaks down the glycosidic bonds
258 resulting in depolymerisation of the cell wall material, thus reducing the Mw of AXs
259 (Margareta and Nyman 2003).

260 Levels of very low Mw (0.79-1.58 kDa) AXs were significantly ($P<0.05$) increased in
261 extruded compared to non-extruded rice bran samples. This could be related to the
262 xylan backbone, which carries more arabinose side chains (Annison et al., 1995),

263 which might be esterified by ferulic acids. It has been reported that extrusion breaks
264 up FA side chains, thus reducing the Mw of AXs (Holguín-Acuña et al. 2008).

265 **Conclusions**

266 Higher percentage levels of low molecular weight AXs were obtained by twin-screw
267 extrusion than by water extraction alone. These findings confirm that extrusion is
268 suitable process to generate low molecular weight AXs for future studies investigating
269 the immunomodulatory properties of AXs and may be practical solution to enrich AXs
270 with most potential health benefits from cereals.

271 **References**

- 272 Annison G, Moughan P, Thomas D (1995) Nutritive activity of soluble rice bran
273 arabinoxylans in broiler diets Br Poult Sci 36:479-488
274
- 275 Broekaert WF, Courtin CM, Verbeke K, Van de Wiele T, Verstraete W, Delcour JA
276 (2011) Prebiotic and other health-related effects of cereal-derived
277 arabinoxylans, arabinoxylan-oligosaccharides, and xylooligosaccharides Crit
278 Rev Food Sci Nutr 51:178-194
- 279 Büchi (2016) Extraction Unit E-812 / E-816 HE/ Technical data sheet. [online]
280 [Accessed June 19th 2016] [http://www.buchi.com/gb-](http://www.buchi.com/gb-en/products/extraction/extraction-unit-e-812-e-816)
281 [en/products/extraction/extraction-unit-e-812-e-816](http://www.buchi.com/gb-en/products/extraction/extraction-unit-e-812-e-816)
- 282 Daou C, Zhang H (2012) Study on functional properties of physically modified dietary
283 fibres derived from defatted rice bran Journal of Agricultural Science 4:85
- 284 Douglas S (1981) A rapid method for the determination of pentosans in wheat flour
285 Food Chem 7:139-145
- 286 Ghoneum M, Matsuura M (2004) Augmentation of macrophage phagocytosis by
287 modified arabinoxylan rice bran (MGN-3/biobran) Int J Immunopathol
288 Pharmacol 17:283-292
- 289 Girhammar U, Nair BM (1992) Certain physical properties of water soluble non-starch
290 polysaccharides from wheat, rye, triticale, barley and oats Food Hydrocolloids
291 6:329-343
- 292 Gualberto D, Bergman C, Kazemzadeh M, Weber C (1997) Effect of extrusion
293 processing on the soluble and insoluble fiber, and phytic acid contents of cereal
294 brans Plant Foods Hum Nutr 51:187-198
- 295 Hashimoto S, Shogren M, Pomeranz Y (1987) Cereal pentosans: their estimation and
296 significance. I. Pentosans in wheat and milled wheat products Cereal chemistry
297 (USA)
- 298 Holguín-Acuña AL, Carvajal-Millán E, Santana-Rodríguez V, Rascón-Chu A,
299 Márquez-Escalante JA, de León-Renova NEP, Gastelum-Franco G (2008)
300 Maize bran/oat flour extruded breakfast cereal: A novel source of complex
301 polysaccharides and an antioxidant Food Chem 111:654-657
- 302 Jeon S-J, Singkhornart S, Ryu G-H (2014) The Effect of Extrusion Conditions on
303 Water-extractable Arabinoxylans from Corn Fiber Preventive nutrition and food
304 science 19:124
- 305 Li W, Hu H, Wang Q, Brennan CS (2013) Molecular features of wheat endosperm
306 arabinoxylan inclusion in functional bread Foods 2:225-237
- 307 Margareta E, Nyman G-L (2003) Importance of processing for physico-chemical and
308 physiological properties of dietary fibre Proc Nutr Soc 62:187-192
- 309 Michniewicz J, Biliaderis C, Bushuk W (1990) Water-insoluble pentosans of wheat:
310 composition and some physical properties Cereal Chem 67:434-439
- 311 Pawar S, Pardeshi I, Borkar P, Rajput M (2014) Optimization of process parameters
312 of microwave puffed sorghum based ready-to-eat (RTE) food Journal of Ready
313 to Eat Food 1:59-68
- 314 Rashid S, Rakha A, Anjum FM, Ahmed W, Sohail M (2015) Effects of extrusion
315 cooking on the dietary fibre content and Water Solubility Index of wheat bran
316 extrudates Int J Food Sci Technol 50:1533-1537
- 317 Rose DJ, Patterson JA, Hamaker BR (2009) Structural differences among alkali-
318 soluble arabinoxylans from maize (*Zea mays*), rice (*Oryza sativa*), and wheat

319 (Triticum aestivum) brans influence human fecal fermentation profiles J Agric
320 Food Chem 58:493-499

321 Santala O, Nordlund E, Poutanen K (2013) Use of an extruder for pre-mixing enhances
322 xylanase action on wheat bran at low water content Bioresource technology
323 149:191-199

324 Saulnier L, Sado P-E, Branlard G, Charmet G, Guillon F (2007) Wheat arabinoxylans:
325 exploiting variation in amount and composition to develop enhanced varieties
326 Journal of Cereal Science 46:261-281

327 Snelders J, Domez E, Delcour JA, Courtin CM (2013) Ferulic acid content and
328 appearance determine the antioxidant capacity of
329 arabinoxylanoligosaccharides J Agric Food Chem 61:10173-10182

330 Svanberg SM, Gustafsson KB, Suortti T, Nyman E-L (1995) Molecular weight
331 distribution, measured by HPSEC, and viscosity of water-soluble dietary fiber
332 in carrots following different types of processing J Agric Food Chem 43:2692-
333 2697

334 Thymi S, Krokida M, Pappa A, Maroulis Z (2005) Structural properties of extruded corn
335 starch Journal of food engineering 68:519-526

336 Vasanthan T, Gaosong J, Yeung J, Li J (2002) Dietary fiber profile of barley flour as
337 affected by extrusion cooking Food Chem 77:35-40

338 Vermaas JV, Petridis L, Qi X, Schulz R, Lindner B, Smith JC (2015) Mechanism of
339 lignin inhibition of enzymatic biomass deconstruction Biotechnology for biofuels
340 8:217

341 Yoo J, Alavi S, Vadlani P, Behnke KC (2012) Soybean hulls pretreated using thermo-
342 mechanical extrusion—hydrolysis efficiency, fermentation inhibitors, and
343 ethanol yield Appl Biochem Biotechnol 166:576-589

344 Zheng X, Li L, Wang X (2011) Molecular characterization of arabinoxylans from hull-
345 less barley milling fractions Molecules 16:2743-2753

346